

CORRESP.

CITATION 2

PATENT SPECIFICATION

(11) 1 578 952

1 578 952

- (21) Application No. 29013/77 (22) Filed 11 July 1977
 (23) Complete Specification filed 17 May 1978
 (44) Complete Specification published 12 Nov. 1980
 (51) INT CL³ C07C 39/16
 (52) Index at acceptance
 C2C 220 227 22Y 30Y 36Y 43X 633 662 699 FG WQ
 (72) Inventor ARIËN KWANTES



(54) PREPARATION OF BISPHENOLS

(71) We, SHELL INTERNATIONALE RESEARCH MAATSCHAPPIJ B.V., a Company organised under the laws of the Netherlands, of 30 Carel Van Bylandtlaan, The Hague, the Netherlands, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:—

The invention is concerned with a process for the preparation of bisphenols and with the bisphenols so prepared.

It is known to prepare bisphenols, e.g. Bisphenol A, by continually reacting, in a reaction zone, at least 2 moles of a phenol having a reactive hydrogen atom with a carbonyl compound in the presence of a substantially insoluble acidic ion-exchange resin. The reaction zone effluent is a mixture of unreacted carbonyl compound, phenol, water, bisphenol and reaction byproducts. Some of the bisphenol and phenol may be in the form of an adduct. It is possible to remove all of the carbonyl compound and water and a part of the phenol from the reaction zone effluent and to recover the bisphenol from the remainder of the reaction zone effluent, e.g. see U.K. specification No. 883,391.

The applicant has now surprisingly found that the concentration of bisphenol in the remainder of the reaction zone effluent may be substantially increased without adversely affecting the properties of the acidic ion-exchange resin or of the recovered bisphenol if a part of the remainder of the reaction effluent is recycled to the reaction zone.

Accordingly, the present invention is concerned with a continuous process for the preparation of bisphenols comprising reacting, in a reaction zone, at least two moles of a phenol having a reactive hydrogen atom with a carbonyl compound in the presence of a substantially insoluble acidic ion-exchange resin, separating the reaction zone effluent into two streams, the first stream comprising unreacted carbonyl compound, water and phenol and the second stream comprising bisphenol, reaction by-products and phenol and recovering bisphenol from the second stream, characterized in that a part of the second stream is recycled to the reaction zone before the bisphenol is recovered therefrom.

The reaction zone may comprise a single reactor or two or more reactors in series. In the case of a multi-reactor reaction zone, suitably all of the phenol is fed to the first reactor and the carbonyl compound is either fed all to the first reactor or divided between the second and possibly further reactors, if any.

As stated above, the reaction zone effluent is separated into two streams. This separation is suitably achieved by the removal, by distillation, of all of the unreacted carbonyl compound and water and a part of the phenol. The reaction zone effluent, depending on the temperature thereof and the pressure used, may be heated or cooled to effect this separation. In the case of a distillation column, the temperature thereof is suitably maintained at a temperature of from 130 to 220°C and a pressure sufficient to completely separate the carbonyl compound and water and a part of the phenol from the reactor zone effluent. In practice the amount of phenol removed is the minimum amount removed during the complete removal of the unreacted carbonyl compound and water. The stream thus obtained, which preferably amounts to from 1 and 10 % w of the reaction zone effluent, may be worked-up and the unreacted carbonyl compound and phenol recycled.

The residue of the separation, i.e. the second stream, comprises bisphenol, reaction by-products and phenol. Suitably the amount of phenol in this stream is from 4 to 15 moles per mole of bisphenol. An important feature of the present

invention is the recycling of a part of this second stream to the reaction zone. In a preferred embodiment of the present invention the recycle ratio, which is the ratio by weight, of the recycle stream to the remainder of the second stream, is in the range of from 0.2:1 to 4:1, with recycle ratios in the range of from 0.5:1 to 2:1 being particularly preferred.

The bisphenol may be recovered from the remainder of the second stream by conventional techniques such as by the removal of the phenol therefrom by evaporation. The bisphenol may also be recovered by crystallization.

The acidic ion-exchange resins for use in the present invention are those whose structures are such as to render the resin substantially insoluble in the reaction medium. Preferred resins contain a plurality of sulphonic acid groups. Such sulphonated ion-exchange resins may be sulphonated styrene-divinylbenzene copolymers and sulphonated phenol-formaldehyde resins. The sulphonated resins are commercially available in a dry or water swollen form and either form may be used in the process. Specific examples of suitable resins are Amberlite IR-120H, Amberlyst 15HO, Dowex 50-X-4, Dowex MSC-1H, Duolite C-26, Permutit QH, Chempro C-20 and Imac C8P/H⁺ (Amberlite, Amberlyst, Dowex, Duolite, Permutit, Chempro and Imac are registered Trade Marks). The exchange capacity of the acidic resin is preferably at least 2.0 meq H⁺/g of dry resin, with exchange capacities in the range of from 3.0 to 5.5 meq H⁺/g of dry resin being particularly preferred.

The acidic ion-exchange resin may be partially modified with a compound having an acidic reacting group and a mercaptan group. Modification may be carried out by either partially esterifying the resin with a mercapto alcohol (e.g. see U.K. Specification No. 937,072) or by partially neutralizing the resin with an alkyl mercaptoamine such as thioethanolamine (e.g. see Belgian Patent No. 589,727 and U.K. Specification No. 1,183,564), precursors of alkyl mercaptoamines such as thiazolidines (e.g. see U.K. Specification No. 1,361,430), cyclomercaptoamines and mercaptoaminocarboxylic acid, as well as thiazolidine precursors of the latter (e.g. see our U.K. Specifications Nos. 1,539,184 and No. 1,539,186. Suitably from 2 to 25%, preferably from 5 to 20%, of the acidic groups are modified. As an alternative to such modification, the reaction may be carried out in the presence of a dissolved sulphur compound as promoter; examples include alkyl mercaptans such as methyl and ethylmercaptan and mercapto-substituted aliphatic carboxylic acids such as 3-mercapto propionic acid.

The reactor may be filled with the acidic ion-exchange resin by any known technique. Such techniques include adding the desired amount of dry resin, water-wet resin or slurry of the resin to the reactor. The resin bed is suitably fixed and is usually supported on one or more grids.

The phenols for use in the present invention should have a reactive hydrogen atom, preferably in the para-position relative to the phenolic hydroxyl group. Such phenols may be substituted by one or more alkyl groups e.g. lower alkyl groups such as methyl or tertiary butyl groups; halogen atoms, such as chlorine atoms, or other non-interfering substituents. Specific examples of phenols include ortho- and meta-cresol; 2,6-dimethylphenol, ortho-sec.butyl phenol, ortho-tert.butyl-phenol; 2,6-di-tert.butylphenol; 1,3,5-xyleneol; tetramethylphenol; 2-methyl-6-tert.butylphenol; ortho-phenylphenol; ortho- and meta-chlorophenol; ortho-bromophenol; 6-chloro-orthocresol and 2,6-dichlorophenol. Phenol itself is the preferred phenol.

The carbonyl compounds used in the process may be aldehydes or ketones with the latter being preferred. Preferred ketones are those having at least one methyl group alpha to carbonyl group or are cyclic ketones. Specific examples include acetone, methyl ethyl ketone, methyl propyl ketone, acetophenone, methyl vinyl ketone and cyclohexanone. Acetone is the preferred ketone. The present invention is particularly suitable for the preparation of 2,2-bis(4-hydroxyphenyl)propane (Bisphenol A).

The molar ratio of phenol to carbonyl compound is at least 2 with a stoichiometric excess of phenol being preferred. Suitable molar ratios are from 3:1 to 50:1, with molar ratios of from 10:1 to 30:1 being preferred. The optimum ratio depends *inter alia* on reaction conditions, e.g. temperature of reaction and desired conversion.

The reaction temperature in the reactor zone may vary between wide limits with a reaction temperature in the range of from 30°C to 120°C being suitable and a reaction temperature in the range of from 40°C to 100°C being preferred.

The reaction time in the reactor zone may also vary between limits and depends *inter alia* on reaction temperature. For example an average total contact

3

1,578,952

3

time of from 3 minutes to 10 hours may be used. The liquid hourly space velocity (LHSV) of the feed may vary between wide limits with velocities in the range of from 0.2 to 40 litres feedstream litre catalyst⁻¹. hour⁻¹ being suitable.

The bisphenols so prepared may be used in a variety of applications such as to prepare anti-oxidants, epoxy resins and polycarbonate resins.

The process will now be illustrated by reference to the drawing accompanying the provisional specification which is a schematic diagram of a preferred embodiment of the present invention.

In this embodiment a feedstream 1 comprising the phenol and the carbonyl compound is continuously fed to the reaction zone R comprising a fixed bed of an acidic ion-exchange resin. The reaction zone R effluent stream 2 is continuously withdrawn and fed to a distillation column D from which an overhead stream 3 comprising all of the carbonyl compound and water and a part of the phenol is continuously withdrawn and worked-up. A bottoms stream 4 comprising bisphenol, reaction by-products and phenol is continuously withdrawn and a part thereof recycled as stream 5 to the reaction zone R. The remaining part thereof, stream 6, is worked-up to recover the bisphenol therefrom.

The invention will now be illustrated with reference to the following Examples.

Example 1

A tubular reactor (150 cm long; 2 cm internal diameter), connected in series with a distillation column (150 cm long; 2 cm internal diameter), was partially filled with an aqueous slurry containing 130 g (dry basis) of a sulphonated styrene/divinylbenzene acidic ion-exchange resin which had been partially neutralized (10%) with thioethanolamine having an exchange capacity of 4.25 meq H⁺/g dry resin, and the water drained-off to form a fixed bed of resin. The reactor was maintained at a temperature of 65°C and the distillation column was maintained at a bottom temperature of 194°C.

A feedstream comprising phenol and acetone was continuously passed through the reactor at a liquid hourly space velocity of 5 litre.litre catalyst⁻¹.hour⁻¹ and the reactor effluent continuously withdrawn and fed to the distillation column from which a top stream (distillate stream) and a bottom stream (recovery stream) were continuously withdrawn. After 120 hours of operation the acetone conversion, on intake, was 52%, and the streams had the following compositions.

	Reactor feedstream (1750 g/h)	Reactor effluent (1750 g/h)	Distillate stream (48 g/h)	Recovery stream (1702 g/h)
	%w	%w	%w	%w
acetone	3.94	1.9	69.1	—
phenol	96.06	89.36	7.7	91.7
diphenylol propane	—	8.0	—	8.2
water	—	0.64	23.2	—
by-products	—	0.1	—	0.1

The recovery stream was worked-up by evaporating the phenol therefrom and the recovered diphenylol propane (DPP) had an ortho/para DPP to para/para DPP ratio of 2.1/97.9 and a colour of 54 Hazen. The amount of phenol that had to be removed by evaporation from the recovery stream was 11.29 g/g of diphenylol propane.

Example 2

Example 1 was repeated with the difference that 60 %w of the bottom stream from the distillation column was continuously recycled (a recycle ratio of 1.5:1) to the reaction zone. The liquid hourly space velocity of the reactor feedstream (fresh feedstream plus recycle stream) was 6 litre.litre catalyst⁻¹.hour⁻¹. After 120 hours of operation the acetone conversion, on intake, was 51%, and the streams had the following compositions.

		1,578,952					
		Reactor feedstream (2064 g/h)	Reactor effluent (2064 g/h)	Distillate stream (48 g/h)	Recycle stream (1217 g/h)	Recovery stream (799 g/h)	
		%w	%w	%w	%w	%w	
5	acetone	3.3	1.68	71	—	—	5
	phenol	86.7	81.1	7	83	83	
	diphenylol propane	9.9	16.5	—	16.8	16.8	
	water	—	0.52	22	—	—	
10	by-products	0.1	0.2	—	0.2	0.2	10

The recovered diphenylol propane had an ortho/para DPP to para/para DPP ratio of 2.2/97.8 and a colour of 54 Hazens. The amount of phenol that had to be removed by evaporation from the recovery stream was 4.9 g/g of diphenylol propane.

15 WHAT WE CLAIM IS:—

1. A continuous process for the preparation of bisphenols comprising reacting, in a reaction zone, at least two moles of a phenol having a reactive hydrogen atom with a carbonyl compound in the presence of a substantially insoluble acidic ion-exchange resin, separating the reaction zone effluent into two streams, the first stream comprising unreacted carbonyl compound, water and phenol and the second stream comprising bisphenol, reaction by-products and phenol and recovering bisphenol from the second stream, characterized in that a part of the second stream is recycled to the reaction zone before the bisphenol is recovered therefrom.
2. A process as claimed in Claim 1, characterized in that the recycle ratio is from 0.2:1 to 4:1.
3. A process as claimed in Claim 1 or 2, characterized in that the reaction zone effluent is separated into two streams by distillation.
4. A process as claimed in any one of Claims 1 to 3, characterized in that the first stream comprises from 1 to 10 %w of the reaction zone effluent.
5. A process as claimed in any one of Claims 1 to 4, characterized in that the acidic ion-exchange resin is a sulphonated styrene-divinylbenzene copolymer which optionally is partially neutralized with an alkyl mercaptoamine.
6. A process as claimed in any one of Claims 1 to 5, characterized in that the molar ratio of phenol to carbonyl compound is from 10:1 to 30:1.
7. A process as claimed in any one of Claims 1 to 6, characterized in that the reaction temperature is from 40°C to 100°C.
8. A process as claimed in Claim 1, substantially as hereinbefore described with particular reference to the Examples.
9. Bisphenols whenever prepared by a process claimed in any one of Claims 1 to 8.

R. C. ROGERS,
Chartered Patent Agent,
Shell Centre,
London, S.E.1 7NA.
Agent for the Applicants.

4.

1

1578952

PROVISIONAL SPECIFICATION

1 SHEET

*This drawing is a reproduction of
the Original on a reduced scale*

